LISTING OF CLAIMS:

This listing of claims will replace all prior versions and listings of claims in the application:

1. (Currently amended) A method for melting inorganic materials, glasses and/or glass-ceramics in a melting unit with cooled walls, in which material to be melted is fed to the melting unit and heated by supplying heating energy, wherein comprising:

selecting a the temperature T_{eff} at which the <u>an</u> energy consumption per unit weight of the <u>inorganic</u> materials to be melted, given a suitably adapted throughput, is at a minimum is determined,

selecting a the temperature of the \underline{a} melt in the melting unit is selected in such a way as to be in a range from T_{eff} - 20% to T_{eff} + 20%, and

selecting a the throughput is selected in such a way as to be adapted to the a required residence time.

2. (Currently amended) The method as claimed in claim 1, wherein the temperature T_{eff} is given by

(1)
$$dE_{tot}/dT = 0 = dE_{N}/dT + dE_{V}/dT$$

$$T=T_{eff}$$

$$T=T_{eff}$$

$$T=T_{eff}$$

where E_N denotes the <u>a</u> useful heat per unit weight of <u>the inorganic</u> materials to be melted and E_V denotes the energy loss per unit weight of <u>the inorganic</u> materials to be melted.

3. (Currently amended) The method as claimed in claim 2, wherein the derivative of the useful heat per unit weight of material to be melted has a derivative according to temperature is given by $dE_n/dT = c_p$, where c_p denotes the \underline{a} specific heat capacity of the melt.

- 4. (Currently amended) The method as claimed in claims 2 and 3, wherein the derivative of claim 2, wherein the energy loss per unit weight of melting material, E_V has a derivative according to temperature is given by $dE_V/dT = k F_0 1/\rho$ $\tau_0 e^{+E/T} + k T F_0 1/\rho \tau_0 (-E/T^2) e^{+E/T}$, where k denotes the \underline{a} total transfer of heat through the walls of the melting unit, $F_0 = F/V$ denotes the \underline{a} surface to volume ratio of the melt, ρ denotes the \underline{a} density of the melt, τ_0 denotes the required residence time at a reference temperature T_0 , and E denotes a constant corresponding to a characteristic activation temperature.
- 5. (Currently amended) The method as claimed in one of the preceding claims, wherein claim 1, further comprising feeding thermal energy is feed directly to the melt.
- 6. (Original) The method as claimed in claim 5, wherein the melt is additionally mixed in the melting unit.
- 7. (Original) The method as claimed in claim 6, wherein the melt is agitated using a stirrer and/or by bubbling.
- 8. (Currently amended) The method as claimed in either of claims 6 and 7, wherein claim 6, further comprising generating a convective flow is generated in the melt.
- 9. (Currently amended) The method as claimed in claim 8, wherein [[a]] the convective flow is produced by setting a viscosity of [[<]] less than 10^3 dPas, preferably of $< 10^2$ dPas, and a melt temperature difference between an inner region of the melt and an outer region of the melt of [[>]] greater than 150 K, preferably > 250 K.
- 10. (Currently amended) The method as claimed in claims 5 to 9, wherein claim 5, further comprising supplying the inorganic materials to be melted is supplied in the form of a batch, which is placed onto the a surface of the melt.

- 11. (Cancelled).
- 12. (Currently amended) The method as claimed in claims 5 to 12 claim 10, wherein the batch is added in the form of pellets.
- 13. (Currently amended) The method as claimed in one of the preceding claims, in which claim 1, further comprising refining the melting material is refined.
- 14. (Currently amended) The method as claimed in claim 13, wherein a further comprising producing a convective flow is produced in the melt.
- 15. (Currently amended) The method as claimed in claim 14, wherein [[a]] the convective flow is produced by setting a viscosity of $< 10^3$ dPas, preferably of < less than 10^2 dPas and a melt temperature difference between an inner region of the melt and an outer region of the melt of > 150 K, preferably > greater than 250 K.
- 16. (Currently amended) The method as claimed in claims 13 to 15, wherein further comprising introducing molten material is introduced into a crucible from one side of the crucible at the <u>a</u> melt bath surface and is discharged again discharging the molten material on an opposite side at the melt bath surface.
- 17. (Currently amended) The method as claimed in one of the preceding claims claim 1, wherein the inorganic materials to be melted is are refined using high-temperature a refining agent.
- 18. (Currently amended) The method as claimed in one of the preceding claims, wherein melting claim 1, further comprising continuously feeding and removing the inorganic materials is continuously feed to and removed from the melt.

- 19. (Currently amended) The method as claimed in claims 1 to $\frac{12}{12}$, wherein the temperature T_{eff} is determined for the melting-down of \underline{a} batch.
- 20. (Original) The method as claimed in claim 19, wherein the temperature T_{eff} is determined for a melt which is additionally mixed.
- 21. (Currently amended) The method as claimed in claim 19, wherein the temperature T_{eff} is determined for a melt which has a viscosity of [[<]] less than 10^3 dPas, preferably of $< 10^2$ dPas and is melted in a unit at which a temperature difference in the melt between the <u>an</u> inner region of the melt and the <u>an</u> outer region of the melt [[is >]] of greater than 150 K, preferably > 250 K.
- 22. (Currently amended) The method as claimed in claims 1 to 4 and 13 to 17, wherein the temperature T_{eff} is determined for the refining of the melt.
- 23. (Currently amended) The method as claimed in claim 22, wherein the temperature T_{eff} is determined for a melt which has a viscosity of [[<]] <u>less</u> than 10^3 dPas, preferably of < 10^4 dPas and is melted in a unit at which a temperature difference in the melt between the <u>an</u> inner region of the melt and the <u>an</u> outer region of the melt [[is >]] of greater than 150 K, preferably > 250 K.
- 24. (Currently amended) The method as claimed in claims 22 and 23, wherein the temperature T_{eff} is determined for a melt in which molten material is introduced into a crucible from one side of the crucible at the \underline{a} melt bath surface and is discharged again on the \underline{a} n opposite side of the crucible at the melt bath surface.
- 25. (Currently amended) The method as claimed in claims 1 to 24, wherein further comprising feeding thermal energy is feed directly to the melt.
- 26. (Currently amended) The method as claimed in claim 25, wherein the thermal energy is fed to the melt by direct conductive heating.

- 27. (Currently amended) The method as claimed in claim 25, wherein the thermal energy is fed to the melt by direct inductive heating.
- 28. (Currently amended) The method as claimed in claims 1 to 27, wherein at least one region of the melt is heated to more than 1 700°C.
- 29. (Currently amended) The method as claimed in one of the preceding claims claim 2, wherein the temperature of at least one region of the melt is selected to be less than or equal to a temperature at which the useful heat and the energy loss per unit weight of the material to be melted are equal.
 - 30 and 31. (Cancelled).
- 32. (Currently amended) The method as claimed in one of the preceding claims, in which claim 1, wherein the required residence time comprises the <u>a</u> melt-down time.
- 33. (Currently amended) The method as claimed in one of the preceding claims, in which claim 1, wherein the required residence time comprises the <u>a</u> refining time.

- 34. (Currently amended) An apparatus for melting inorganic materials, glasses and glass-ceramics, for carrying out the method as claimed in one of claims 1 to 33, which apparatus comprises comprising:
 - a melting unit with cooled walls,
 - a device for supplying material to be melted to the melting unit, and
- a device for the direct heating of the material to define a melt, and which apparatus also includes

a device for setting a temperature which is at least $T_{\rm eff}$ – 20% to $T_{\rm eff}$ + 20% in at least one region of the melt, the temperature $T_{\rm eff}$ being given by the temperature at which the <u>an</u> energy consumption per unit weight of the material to be melted, with a throughput which is suitably adapted to the <u>a required</u> residence time required at a given temperature, is at a minimum, and

a device for adapting the relative throughput of material to be melted to the required residence time in the melt.

- 35. (Original) The apparatus as claimed in claim 34, wherein the melting unit with cooled walls comprises a skull crucible.
- 36. (Currently amended) The apparatus as claimed in claim 34 or 35, which includes <u>further comprising</u> a stirrer for agitating the melt.
- 37. (Currently amended) The apparatus as claimed in one of claims 34 to 36, which includes <u>further comprising</u> at least one nozzle for introducing bubbling gas <u>to the melt</u>.
- 38. (Currently amended) The apparatus as claimed in one of claims 34 to 37, wherein the device for the direct heating of the melt comprises a device for the conductive heating of the melt.

39-46. (Cancelled).

- 47. (Currently amended) The A glass comprising as claimed in claim 46, preferably produced by the method as claimed in one of claims 1 to 33, wherein the a ratio of Sn²⁺ to Sn_T has having a value of greater than 0.25, preferably greater than 0.35, particularly preferably greater than 0.45.
- 48. (Currently amended) [[A]] The glass product producible by the method as claimed in one of claims 1 to 33 claim 47, wherein the value is greater than 0.35.
- 49. (Currently amended) The glass product as claimed in claim 48, preferably produced by the method as claimed in one of claims 1 to 33 <u>47</u>, wherein the ratio of Sn²⁺ to Sn_T has a value of greater than 0.25, preferably greater than 0.35, particularly preferably is greater than 0.45.